

# Heat and Mass Transfer Investigation of Oldroyd-B Fluid in a Curved Symmetric Channel

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## ABSTRACT

This study analyzed the mass/heat transfer of the Oldroyd-B liquid model by peristaltic mechanism in the appearance of an electrically conductive magnetic parameter through a curved channel. The governing equation of the Oldroyd-B liquid model is formulated and lengthy equations are shortened by the considerations of long wavelengths and very small Reynolds number approximations. The exact results were calculated. The impact of various fluid parameters in fluid's velocity, concentration, temperature, Sherwood number, and Nusselt number are illustrated through the computational mathematical software Matlab, and the stream function is computed through Mathematica. The impact of important parameters of the relevant fluids was discussed.

**Keywords:** Peristaltic flow, Oldroyd-B fluid, Curved channel, Magnetic field

## 1. INTRODUCTION

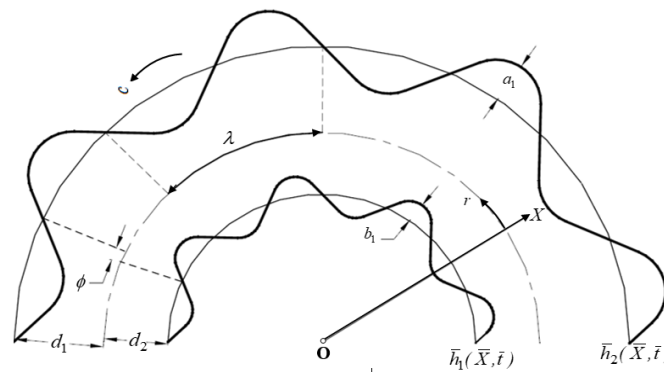
Peristaltic motion is a phenomenon where fluid motion occurs when a progressive wave of expansion or contraction of the area extends along the distensible tube or channel. This mechanism is widely used in biomedical, engineering, and other industries. Some of the applications in industries are plastics manufacturing, locomotion of worms, toxic liquid movement in the nuclear industry, ketchup, food processing, the performance of lubricants, sanitary fluid transportation, finger and roller pumps. In physiology, in the vasomotion of venules, urine movement to bladder from kidney, capillaries, and arterioles, swallowing food via the esophagus, etc. Latham [1] started the peristaltic flow of fluid motion in two-dimensional Cartesian coordinates in his thesis. Burns and Parkes [2], Shapiro et al. [3] both expand on this study. To simplify the governing equations, they used long wavelength and small Reynolds number assumptions. Asymmetric channels with Newtonian fluid were examined by Mishra and Rao [4]. The magnetic field of the peristaltic mechanism plays a major role in bio-engineering and medicine. Some of the applications are in the development of magnetic tracers, bleeding reductions during surgeries, drug transport, hyperthermia, magnetic devices built for cell separation, etc. Heat transfer of fluid transport through peristalsis works in numerous applications in oxygenation, food processing, tissue conduction, hemodialysis, and radiation between the environment and its surroundings. Concentration (Mass) transfer involves important applications in the diffusion of chemical impurities, separation membrane and process of combustion, the study of warm salty springs in the ocean, etc. Some of the investigations based on the peristaltic transport of various liquid models with mass/heat transfer under the involvement of various body forces in different geometries are presented [5-23]. Nevertheless, the majority of the previously described research on peristalsis use flat or straight channels, which may not be sufficient when considering flows through glandular and physiological conduits. We encounter curved geometries in physical and industrial processes, where curvilinear coordinates must be taken into account in order to counter challenging mathematical statements. Sato et al. [24] initially explored the peristaltic motion of liquid particles in two-dimensional Cartesian coordinates through the curved channel. Some studies of related to curved channel presented in [25-40].

The present study aims to construct upon the investigations to analyze mass/heat transfer of Oldroyd-B fluid with a magnetic field under peristalsis. We have tried to construct a mathematical formulation to

provide a realistic manifestation of the blood flow. So, the fluid motion is taken into account in curved channels because many of the glandular ducts and arteries are curved. No investigations have been discussed yet by considering the Oldroyd-B fluid model with mass/heat transfer investigations under the impact of the magnetic field. Therefore, the relevant mathematical formulation is made based on the flow pattern and the equations are abridged with the help of lubrication theory approximation. Reduced equations of the velocity, energy and mass transfer equations are exactly solved. The results are discussed for various values of involved pertinent parameters through the graphs.

**2. Mathematical structure**

A2-dimensional incompressible Oldroyd-B liquid in a curved geometry with uniform half-width  $a$ , center  $O$ , and radius  $\Upsilon$ . The deformable channel walls are propagated by sinusoidal waves with velocity  $c$  See Figure 1.



**Figure 1.** Flow geometry of the curved channel.

The shape of the wave is represented as [24]

$$\begin{aligned} \bar{h}_1 &= -a - b \sin \left[ \frac{2\pi}{\lambda} (x - ct) \right] \\ \bar{h}_2 &= a + b \sin \left[ \frac{2\pi}{\lambda} (x - ct) \right] \end{aligned} \tag{1}$$

where  $\lambda, t, b$  are the wavelength, time, wave amplitude.

In the radial direction, the fluid particle is electrically conducting with an externally applied magnetic field  $B$ .

$$B = \left( \frac{B_0}{r + \Upsilon}, 0, 0 \right) \tag{2}$$

In which  $B_0$  is the magnetic field strength, Ohm's law yields the subsequent expression.

$$J \times B = \left( 0, -\frac{\sigma B_0^2 U}{(r + \Upsilon)^2}, 0 \right) \tag{3}$$

Where  $J, \sigma$  are current density, electrical conductivity.

The constitutive equations for the Oldroyd-B fluid model are given by [37]

$$\begin{aligned} \tau &= -pI + S \\ \left( 1 + \lambda_2 \frac{d}{dt} \right) S &= \mu \left( 1 + \lambda_2 \frac{d}{dt} \right) A_1 \\ A_1 &= L + L^T, L = \text{grad } V \end{aligned} \tag{4}$$

The component of the extra tense tensor  $S$  can be described as follows:

$$\begin{aligned} \left(1 + \lambda_1 \left(\frac{\partial}{\partial t} + \frac{\Upsilon u}{r + \Upsilon} \frac{\partial}{\partial x} + v \frac{\partial}{\partial r}\right)\right) S_{rr} &= 2\mu \left(1 + \lambda_2 \left(\frac{\partial}{\partial t} + \frac{\Upsilon u}{r + \Upsilon} \frac{\partial}{\partial x} + v \frac{\partial}{\partial r}\right)\right) \frac{\partial v}{\partial r}, \\ \left(1 + \lambda_1 \left(\frac{\partial}{\partial t} + \frac{\Upsilon u}{r + \Upsilon} \frac{\partial}{\partial x} + v \frac{\partial}{\partial r}\right)\right) S_{xr} &= \mu \left(1 + \lambda_2 \left(\frac{\partial}{\partial t} + \frac{\Upsilon u}{r + \Upsilon} \frac{\partial}{\partial x} + v \frac{\partial}{\partial r}\right)\right) \left(\frac{\partial u}{\partial r} + \frac{\Upsilon u}{r + \Upsilon} \frac{\partial v}{\partial x} - \frac{u}{r + \Upsilon}\right), \\ \left(1 + \lambda_1 \left(\frac{\partial}{\partial t} + \frac{\Upsilon u}{r + \Upsilon} \frac{\partial}{\partial x} + v \frac{\partial}{\partial r}\right)\right) S_{xx} &= 2\mu \left(1 + \lambda_2 \left(\frac{\partial}{\partial t} + \frac{\Upsilon u}{r + \Upsilon} \frac{\partial}{\partial x} + v \frac{\partial}{\partial r}\right)\right) \left(\frac{\Upsilon}{r + \Upsilon} \frac{\partial u}{\partial x} + \frac{v}{r + \Upsilon}\right), \end{aligned}$$

where  $I, \tau, \mu, p, \lambda_1, \lambda_2, S$  are the Identity tensor, Cauchy stress tensor, dynamic viscosity, pressure, relaxation and the retardation times, extra stress tensor, and  $A_1$  is a first Rivlin Ericksen tensor. The equations governing for an Oldroyd-B fluid model is defined as

$$\frac{\partial v}{\partial r} + \frac{\Upsilon}{\Upsilon + r} \frac{\partial u}{\partial x} + \frac{v}{\Upsilon + r} = 0 \tag{6}$$

$$\rho \left(\frac{\partial v}{\partial t} + v \frac{\partial v}{\partial r} + \frac{\Upsilon u}{\Upsilon + r} \frac{\partial v}{\partial x} - \frac{u^2}{r + \Upsilon}\right) = -\frac{\partial P}{\partial r} + \frac{\mu}{r + \Upsilon} \frac{\partial S_{rr}}{\partial r} + \frac{\mu \Upsilon}{r + \Upsilon} \frac{\partial S_{xr}}{\partial x} - \frac{\mu S_{xx}}{r + \Upsilon} \tag{7}$$

$$\rho \left(\frac{\partial u}{\partial t} + v \frac{\partial u}{\partial r} + \frac{\Upsilon u}{\Upsilon + r} \frac{\partial u}{\partial x} - \frac{uv}{r + \Upsilon}\right) = -\frac{\Upsilon}{r + \Upsilon} \frac{\partial P}{\partial x} + \mu \frac{\partial S_{rx}}{\partial r} + \frac{\mu \Upsilon}{r + \Upsilon} \frac{\partial S_{xx}}{\partial x} - \frac{\sigma B_0^2 u}{(r + \Upsilon)^2} \tag{8}$$

$$\begin{aligned} \rho c_p \left(\frac{\partial T}{\partial t} + v \frac{\partial T}{\partial r} + \frac{\Upsilon u}{\Upsilon + r} \frac{\partial T}{\partial x}\right) &= \kappa_t \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r + \Upsilon} \frac{\partial T}{\partial r} + \left(\frac{\Upsilon}{r + \Upsilon}\right) \frac{\partial^2 T}{\partial x^2}\right) \\ &+ \frac{Dk_t}{C_s} \left(\frac{\partial^2 C}{\partial r^2} + \frac{1}{r + \Upsilon} \frac{\partial C}{\partial r} + \left(\frac{\Upsilon}{r + \Upsilon}\right) \frac{\partial^2 C}{\partial x^2}\right) + tr(LS) \end{aligned} \tag{9}$$

$$\begin{aligned} \left(\frac{\partial C}{\partial t} + v \frac{\partial C}{\partial r} + \frac{\Upsilon u}{\Upsilon + r} \frac{\partial C}{\partial x}\right) &= D \left(\frac{\partial^2 C}{\partial r^2} + \frac{1}{\Upsilon + r} \frac{\partial C}{\partial r} + \left(\frac{\Upsilon}{\Upsilon + r}\right) \frac{\partial^2 C}{\partial x^2}\right) \\ &+ \frac{Dk_t}{T_m} \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r + \Upsilon} \frac{\partial T}{\partial r} + \left(\frac{\Upsilon}{r + \Upsilon}\right) \frac{\partial^2 T}{\partial x^2}\right). \end{aligned} \tag{10}$$

Here  $\rho, \nu, T, C$  are the density, kinematic viscosity, temperature, concentration,  $c_p, C_s, T_m, \kappa_t, D, k_t$  are the specific heat, concentration susceptibility, mean fluid temperature, thermal conductivity, mass diffusivity coefficient, thermal diffusion ratio. Here  $L = \text{grad } V$ . In the fixed frame  $(r, x)$  the fluid velocity is not steady. For steady flow analysis, the fixed frame is transformed into the wave frame  $(\bar{r}, \bar{x})$  using the Galilean transformations [40].

$$\bar{r} = r, \bar{x} = x - ct, \bar{v} = v, \bar{u} = u - c \tag{11}$$

We Introducing the following dimensionless quantities are

$$\begin{aligned} \eta = \frac{\bar{r}}{a}, v^* = \frac{\bar{v}}{c}, p^* = \frac{a^2}{\mu \lambda c} \bar{p}, \delta = \frac{a}{\lambda}, S_{ij}^* = \frac{aS_{ij}}{c\mu}, \psi^* = \frac{\psi}{ca}, x^* = \frac{\bar{x}}{\lambda}, u^* = \frac{\bar{u}}{c}, \\ E = \frac{c^2}{T_0 c_p}, k = \frac{\Upsilon}{a}, H^2 = \frac{\sigma B_0^2}{\mu}, Sr = \frac{\rho D \kappa_t T_0}{\mu T_m C_0}, Du = \frac{D \kappa_t C_0}{\mu C_s C_p T_0}, Pr = \frac{\mu C_0}{\kappa_t}, \phi = \frac{C - C_0}{C_0}, \\ Br = E Pr, Sc = \frac{\mu}{\rho D}, \theta = \frac{T - T_0}{T_0}, Br = \frac{\mu c^2}{\kappa(T_0 - T_1)}, Re = \frac{\rho ca}{\mu} \end{aligned} \tag{12}$$

And the dimensionless stream function

$$u = -\frac{\partial \psi}{\partial \eta}, v = \delta \frac{k}{\eta + k} \frac{\partial \psi}{\partial s} \tag{13}$$

Applying Eq. (11) into Eqs. (6)-(10) and then with the help of Eqs. (12) and (13), consideration of tiny Reynolds number, long wavelength, Eq. (6) is satisfied and Eqs. (7)– (10) after removing (\*) becomes

$$\frac{\partial p}{\partial \eta} = 0, \quad (14)$$

$$-\frac{k}{\eta+k} \frac{\partial p}{\partial x} + \frac{1}{(\eta+k)^2} \frac{\partial}{\partial \eta} \left( (\eta+k)^2 S_{rx} \right) + \frac{(\psi_\eta - 1) H^2}{(\eta+k)^2} = 0, \quad (15)$$

$$\frac{\partial^2 \theta}{\partial \eta^2} + \frac{1}{\eta+k} \frac{\partial \theta}{\partial \eta} + \text{Pr} \text{Du} \left( \frac{\partial^2 \varphi}{\partial \eta^2} + \frac{1}{\eta+k} \frac{\partial \varphi}{\partial \eta} \right) + \text{Br} \left( -\psi_{\eta\eta} + \frac{\psi_\eta}{\eta+k} - \frac{1}{r+k} \right) S_{xr} = 0, \quad (16)$$

$$\frac{1}{\text{Sc}} \left( \frac{\partial^2 \varphi}{\partial \eta^2} + \frac{1}{\eta+k} \frac{\partial \varphi}{\partial \eta} \right) + \text{Sr} \left( \frac{\partial^2 \theta}{\partial \eta^2} + \frac{1}{\eta+k} \frac{\partial \theta}{\partial \eta} \right) = 0, \quad (17)$$

In above expressions,  $Re, \delta, E, Br, Sc, Sr, Du, Pr, H$  are Reynolds number, wave number, Eckert number, Brinkmann number, Schmidt number, Soret number, Dufour number Prandtl number, Hartmann number.

Eq. (14) shows the pressure is not dependent of  $\eta$ .

$$\frac{\partial}{\partial \eta} \left[ \frac{1}{(\eta+k)k} \frac{\partial}{\partial \eta} \left( (k+\eta)^2 S_{rx} \right) + \frac{H^2 (\psi_\eta - 1)}{k(\eta+k)} \right] = 0, \quad (18)$$

$$\text{Where } S_{rx} = S_{xr} = \left( -\psi_{\eta\eta} + \frac{\psi_\eta}{\eta+k} - \frac{1}{\eta+k} \right), \quad (19)$$

The corresponding boundaries are

$$\psi = -\frac{F}{2}, \quad \frac{\partial \psi}{\partial \eta} = -1, \theta = 0, \varphi = 0 \text{ at } h_1 = -1 - \varepsilon \sin(x),$$

$$\psi = \frac{F}{2}, \quad \frac{\partial \psi}{\partial \eta} = -1, \theta = 1, \varphi = 1 \text{ at } h_2 = 1 + \varepsilon \sin x,$$

(20)

In the fixed frame the volume flow rate in the dimensional form as [26]

$$Q = \int_{\bar{h}_1}^{\bar{h}_2} \bar{U} d\bar{R} \quad (21)$$

here  $\bar{h}_2$  and  $\bar{h}_1$  are functions of  $\bar{t}$  and  $x$ . The wave frame is as follows

$$q = \int_{\bar{h}_1}^{\bar{h}_2} \bar{u} dr \quad (22)$$

where  $\bar{h}_2$  and  $\bar{h}_1$  are functions of  $\bar{x}$  alone. Eqs (21) and (22) can be presented as

$$Q = ch_2 - ch_1 + q \quad (23)$$

the average volume flow rate ( $T = \lambda / c$ ) is

$$\bar{Q} = \frac{1}{T} \int_0^T Q dt = \frac{1}{T} \int_0^T (ch_2 - ch_1 + F) dt = q + 2ac, \quad (24)$$

the mean flow  $\Theta$  in the fixed frame and  $q$  in the wave frame is defined as

$$\Theta = \frac{\bar{Q}}{ac}, \quad F = \frac{q}{ac} \quad (25)$$

Therefore, applying eq. (25) into eq. (24) we get

$$\Theta = F + 2 \quad (26)$$

**3. Solution of the problem**

The solution of Eqs.(18), (16) and (17) with Eq.(20) we get.

$$\psi = c_1 \frac{(\eta + k)^{1+\sqrt{1+H^2}}}{1+\sqrt{1+H^2}} + c_2 \frac{(\eta + k)^{1-\sqrt{1+H^2}}}{1-\sqrt{1+H^2}} + c_3 (2k\eta + \eta^2) + c_4 + \frac{\eta + k}{1+H^2} \quad (27)$$

$$\theta = c_{11} \log(\eta + k) + c_{12} + \frac{Br}{(1+H^2)^2 (-1 + Pr Du Sc Sr)} \left[ (l_1^2 + 2H^2 l_1) \frac{(\eta + k)^{\sqrt{1+H^2}}}{1+H^2} + (l_2^2 + H^2 l_2) \frac{(\eta + k)^{-\sqrt{1+H^2}}}{1+H^2} + \frac{2l_1 l_2}{\eta + k} + \frac{H^4 \log(\eta + k)^2}{2} \right]$$

(28)

$$\varphi = c_{21} \log(\eta + k) + c_{22} - \frac{Br Sc Sr}{(1+H^2)^2 (-1 + Pr Du Sc Sr)} \left[ (l_1^2 + 2H^2 l_1) \frac{(\eta + k)^{\sqrt{1+H^2}}}{1+H^2} + (l_2^2 + H^2 l_2) \frac{(\eta + k)^{-\sqrt{1+H^2}}}{1+H^2} + \frac{2l_1 l_2}{\eta + k} + \frac{H^4 \log(\eta + k)^2}{2} \right] \quad (29)$$

Where constants appeared in the above equations are lengthy expressions. So, it is given in the appendix.

The  $z$  and  $Sh$  for both the walls are defined as[7]

$$z = \frac{\partial h_i}{\partial x} \left( \frac{\partial \theta}{\partial \eta} \right)_{\eta=h_i}, \quad i = 1, 2 \text{ (heat transfer coefficient)} \quad (30)$$

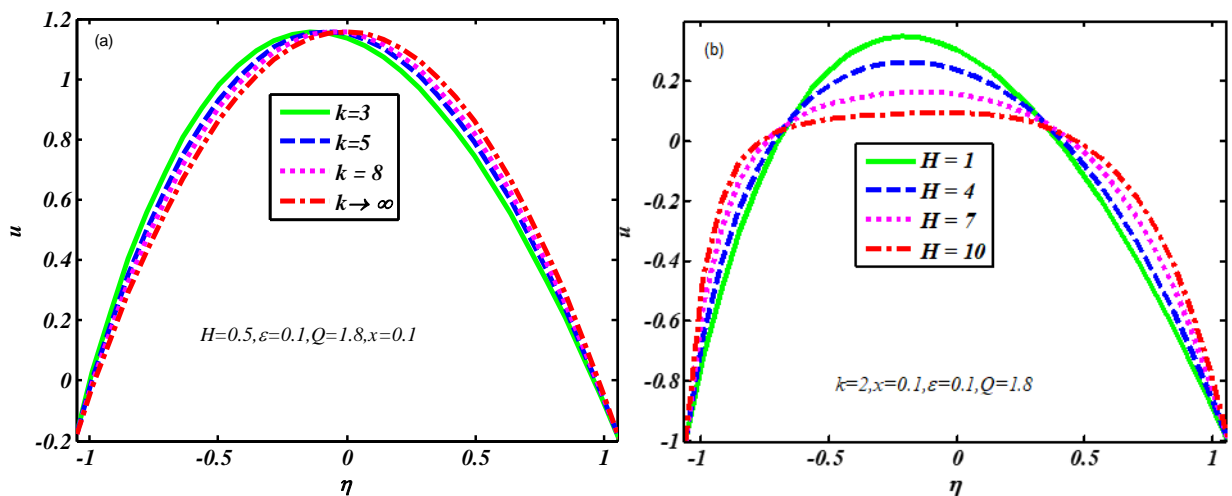
$$Sh = \frac{\partial h_i}{\partial x} \left( \frac{\partial \varphi}{\partial \eta} \right)_{\eta=h_i}, \quad i = 1, 2 \text{ (Sherwood number)} \quad (31)$$

**4. RESULT AND DISCUSSION**

In this part, variations of velocity,  $\varphi$ ,  $\theta$ ,  $z$ ,  $Sh$  and streamlines are examined for the different values of the involved parameter.

**4.1. Velocity distribution**

Velocity distributions are presented in Fig.2(a) and (b). The result of the variations of velocity for the curvature parameter is presented in Fig.2(a).

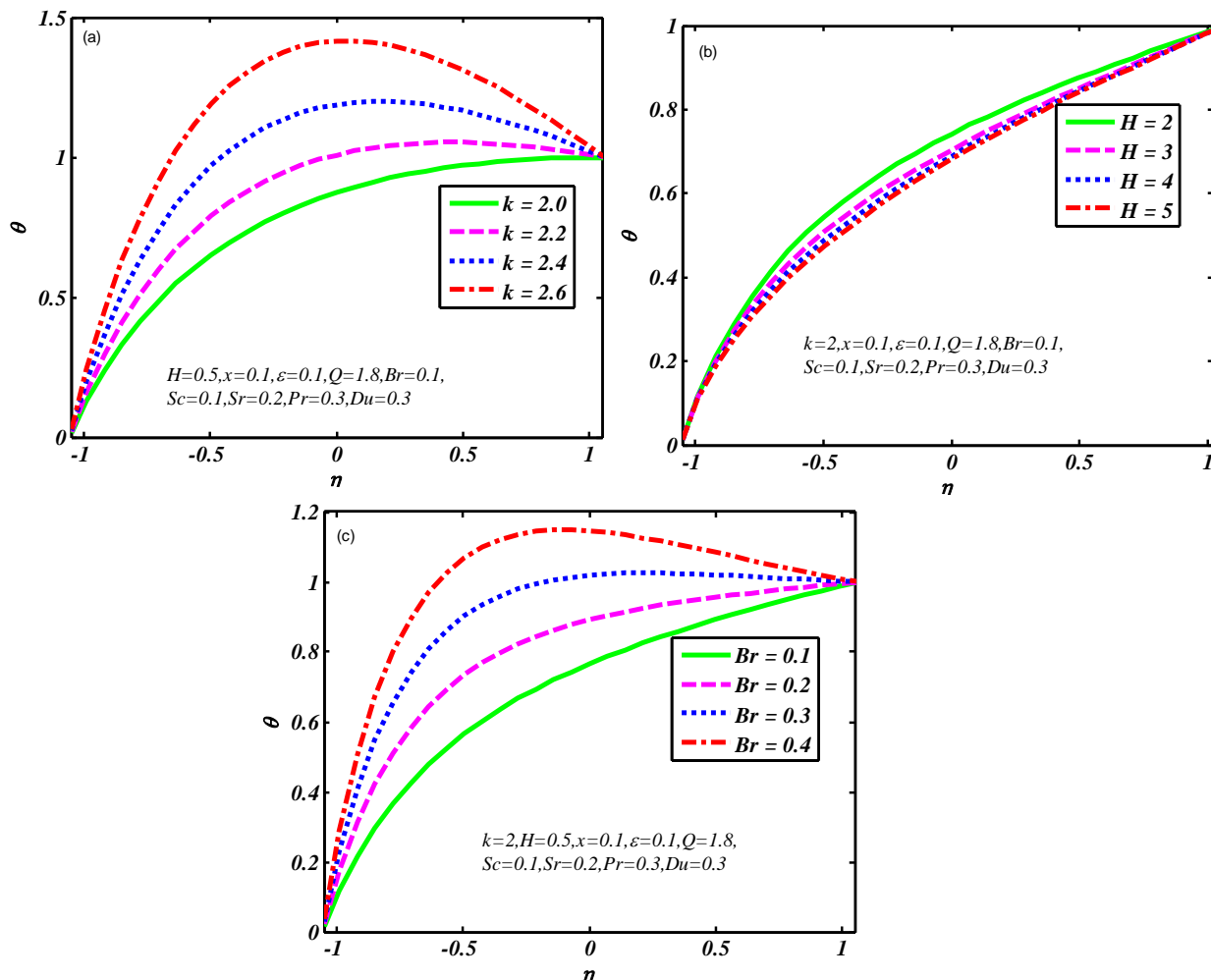


**Figure 2.** Velocity Distribution

This graph indicates, the velocity profile seems asymmetric in the curved channel, for a larger  $k$  the velocity profile is symmetric. Fig.2(b), presented for velocity variation of  $H$ . This figure shows, the velocity of the liquid reduces for a large value of  $H$ . Actually, Lorentz force produce resistance in the fluid flow field. Furthermore, increasing the magnetic field strength provides an obstruction for the high-pressure gradient to travel inside the curved channel. Consequently, the magnetic field seems to be a delaying factor in the radial direction for fluid movement. Magnetic fields have an inverse behaviour and are beneficial in the treatment of disorders such as migraine headaches, joint difficulties, depression, cancer, etc.

**4.2. Temperature and concentration distribution**

In this subsection, we have analyzed the temperature distribution for involved fluid parameters like curvature parameter  $k$ , Brinkman number  $Br$  and  $H$ . The concluded results of Fig. 3(a)



**Figure 3.** Temperature Distribution

manifest raises the temperature towards straight channel. The temperature of the liquid diminishes for the magnetic parameter boosts see Fig. 3(b). This could be due to the flow being affected by the ohmic heating of the magnetic field. Moreover, a strong magnetic field is produced for larger  $H$ , which cools the fluid by removing heat and generating current in the motors. Fig. 3(c). The temperature profile went up to large Brinkman number ( $Br$ ) values. Taking into account that the  $Br$  suggests effects on viscous dissipation that cause heat to be produced inside the channel.

Fig.4. (a-e) plotted for concentration profiles against the pertinent involved dimensionless parameters. From the above mentioned Figures, we noticed that reduction behavior of ( $\phi$ ) concentration concluded

towards curvature parameter  $k$  see Fig.4(a), Hartmann number  $H$  Fig.4(b) and Brinkmann number  $Br$  Fig.4(c).

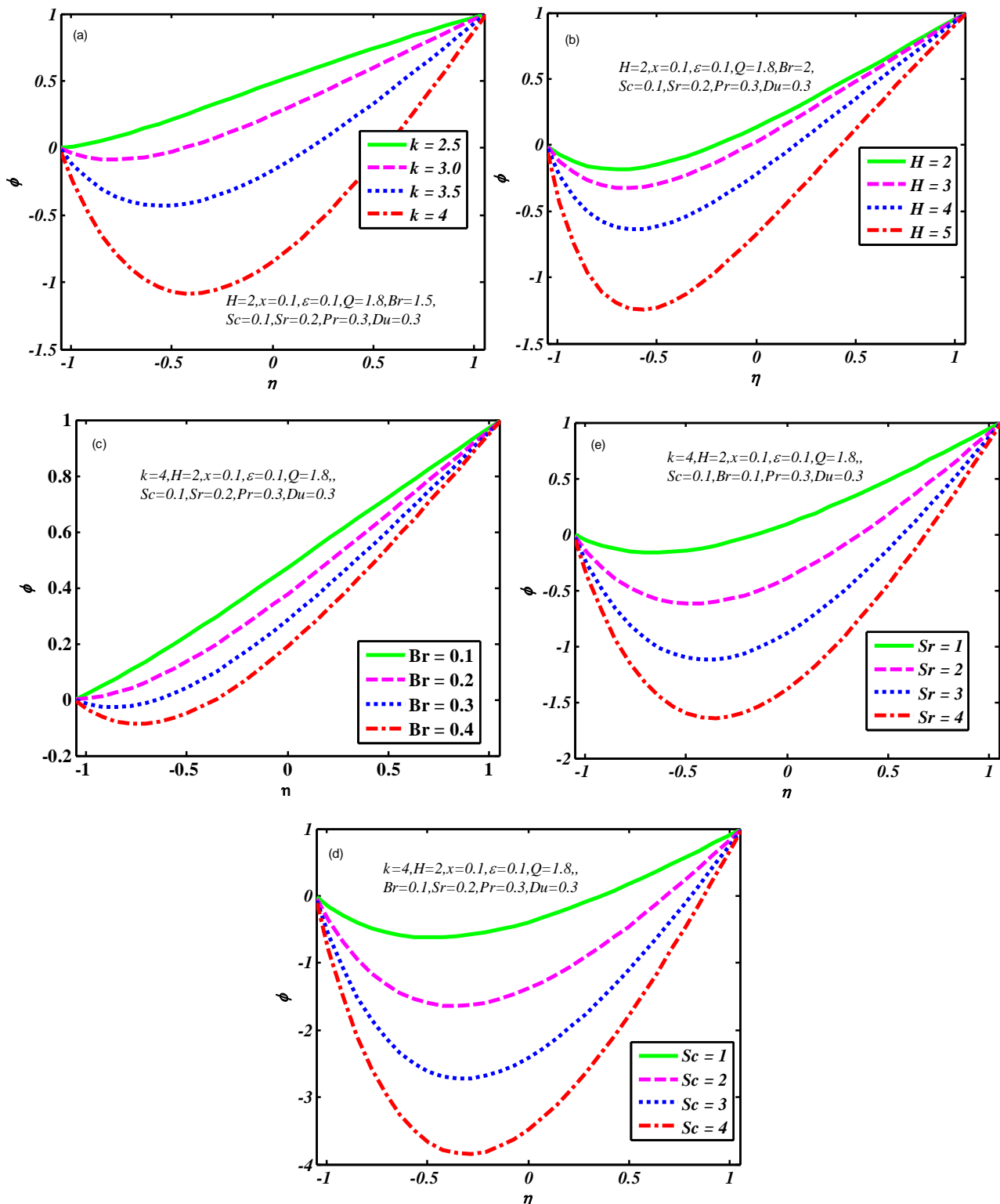


Figure 4. Concentration Distribution

Schmidt number  $Sc$  is the ratio between momentum and mass diffusivity. Therefore, it is perceivable from Fig. 4(d) that concentration reduces as  $Sc$  boosted. Similar trend concluded for greater  $Sr$  values see Fig.4(e).

4.3. Heat transfer coefficient and Sherwood number

Fig. 5. (a-c) presented for the behavior of heat transfer coefficient against  $k, H, Br, Sc$  and  $Sr$ . From this diagram, we clarify that due to the peristaltic mechanism, the coefficient of thermal transfer profile is oscillatory behavior.

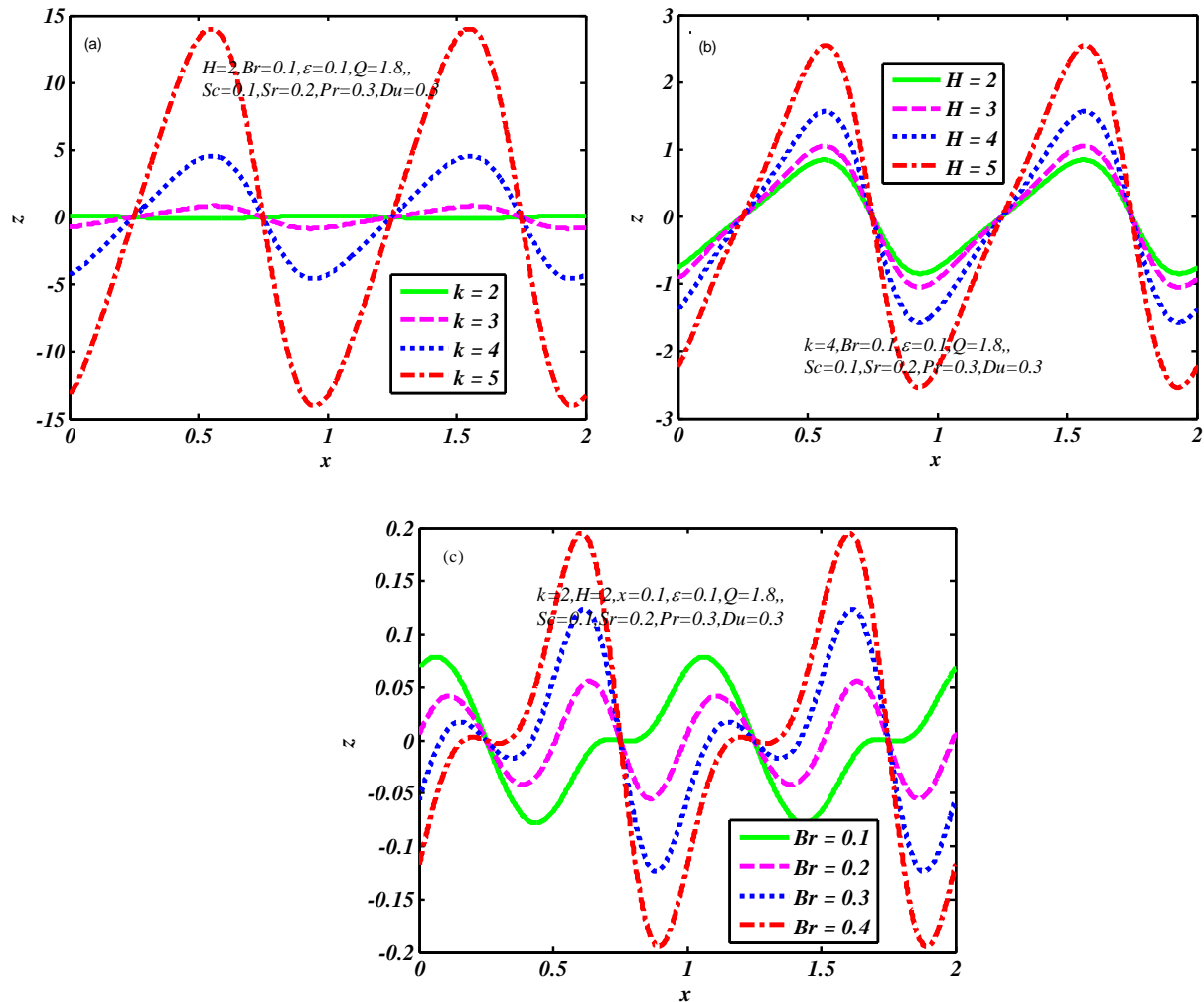


Figure 5. Variation of Heat Transfer Co-efficient  $z$ .

The magnitude of heat transfer  $h_x$  coefficient increases in the region  $(0.25 < x < 0.75)$  and  $(1.25 < x < 1.75)$  decreases in the region  $(0.75 < x < 1.25)$ . Similar behavior of  $h_x$  concluding for Sherwood number. ie., oscillatory behavior. But increasing values of  $k, H, Br, Sc$  and  $Sr$  the Sherwood number reduces in the region  $(0.25 < x < 0.75)$  and  $(1.25 < x < 1.75)$  raises in the region  $(0.75 < x < 1.25)$  see the Figs.6.(a-e).



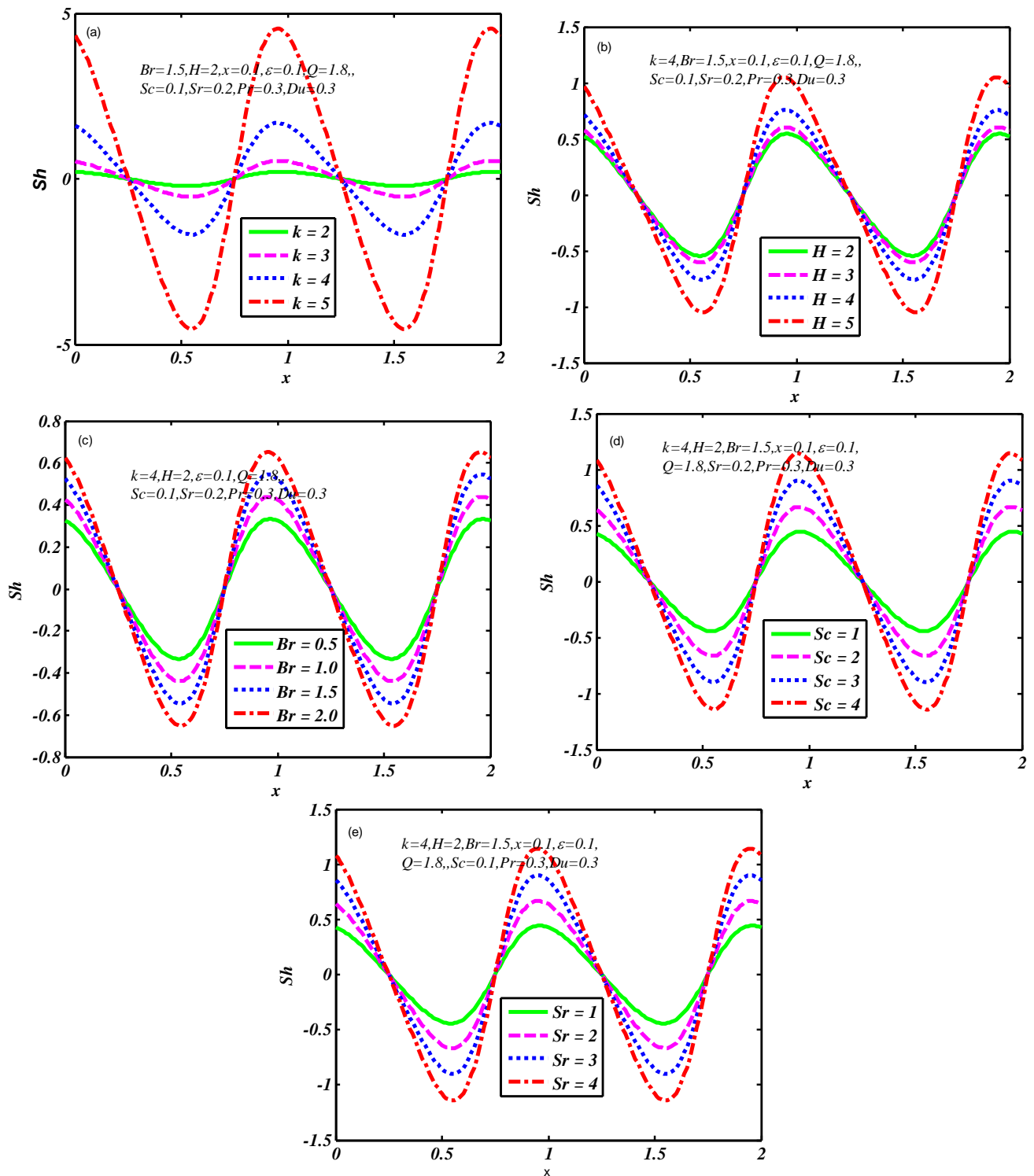
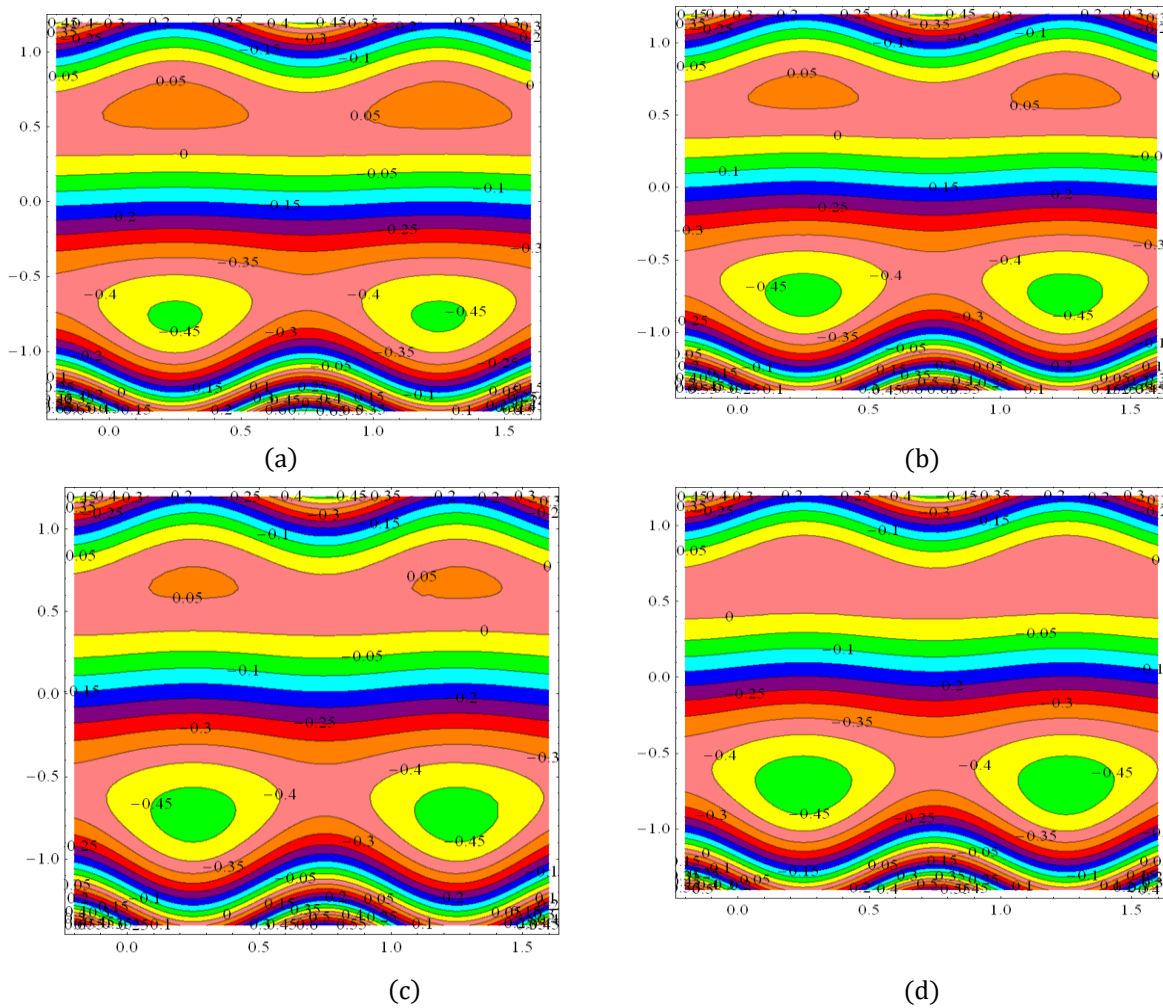


Figure 6. Sherwood Number Variation

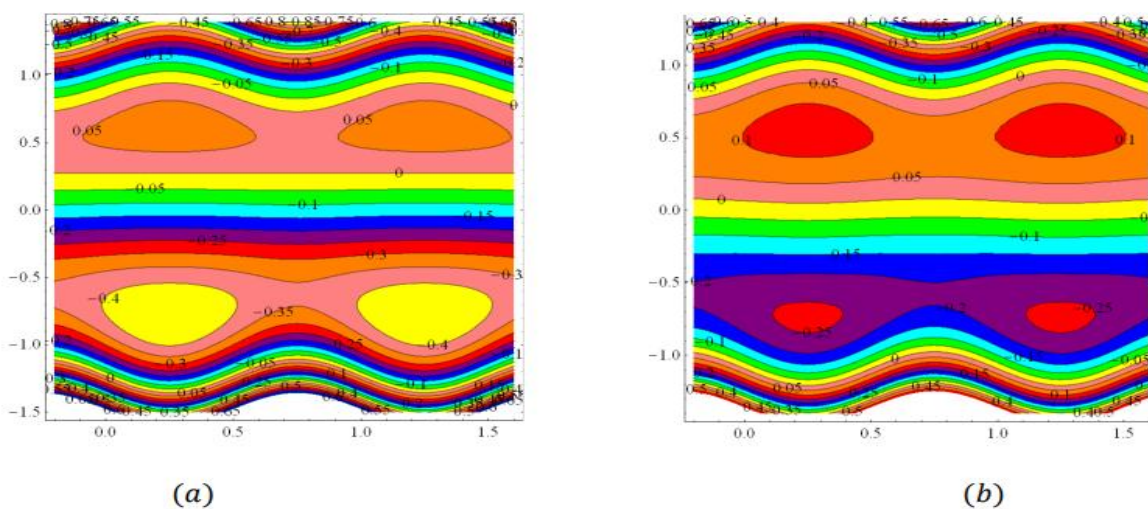
#### 4.4. Trapping Results

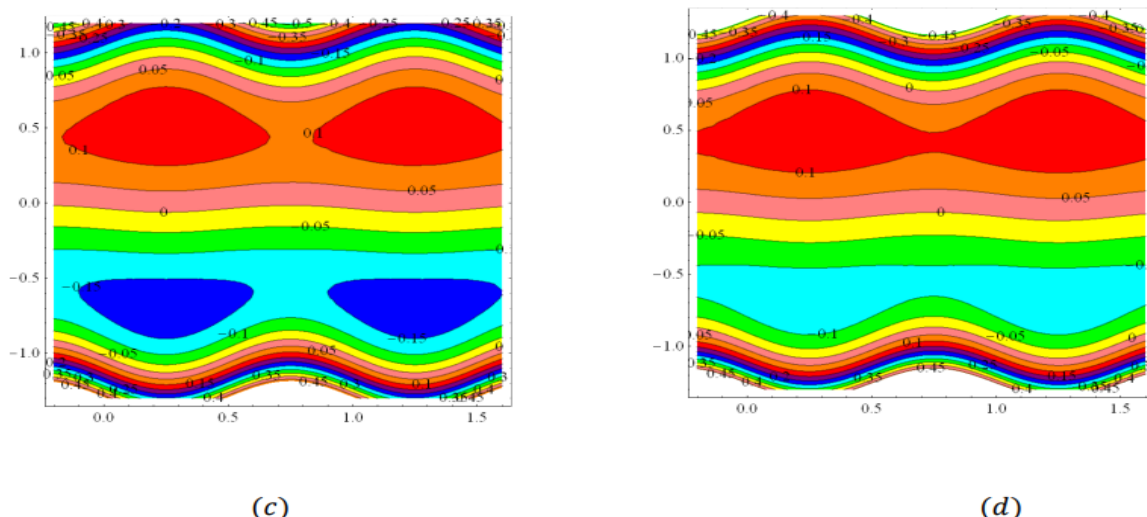
The trapping pattern is another important mechanism to analyze the flow of fluid. Peristaltic transport can be investigated by examining a closed contour of streamlines at various wave amplitudes and average time flow rates. The process is known as trapping. From a physiological standpoint, fluids might become trapped as a result of continuous smooth border movements, which is good for adequately propelling the biological working fluid from one location to another. With the proper extension, the working organs can be kept alive for an extended period of time without complications. Therefore, trapping phenomena can be studied by displaying the stream functions relative to  $k$  and  $H$ . Fig. 7. (a-d) presented for streamlines

for  $k$  variation. It is concluded that the dimensions of the trapped bolus decrease in the upper peristaltic wall, also increase in the lower wall at high curvature, with the bolus disappearing in the upper wall to the curved to straight channel. Fig. 8. (a-d) depicts the size of the trapped bolus in the upper wall increases at the same time the lower wall decreases with the increasing amount of  $H$ .



**Figure 7.** Streamlines for (a)  $k = 2$ , (b)  $k = 4$ , (c)  $k = 6$ , (d)  $k = 8$  the other parameters are  $x = 0.1, Q = 1.8, H = 2, \varepsilon = 0.1$





**Figure 8.** Streamlines for (a)  $H = 2$ , (b)  $H = 3$ , (c)  $H = 4$ , (d)  $H = 5$  the other parameters are  $x = 0.1, Q = 1.8, k = 3, \varepsilon = 0.1$

**5. CONCLUSION**

In this paper we analyzed the mass and energy transfer of the Oldroyd-B liquid through a symmetrical curved channel under peristaltic mechanism. The key findings are presented below

1. Parabolic nature concluded in the velocity profile and also symmetric in the planner channel, but non-symmetric in the curved channel.
2. Reduces the velocity towards the massive quantity of  $H$
3. The enhanced amount of  $k, H, Br$  temperature raises, but concentration reduces. The same reduction concluded for raising the values of  $Sc, Sr$
4.  $h_x, Sh$  Profiles are oscillatory behavior concluded.  $h_x$  Increases but  $Sh$  decreases in the upper walls for small to large values  $k, H, Br$  and  $k, H, Br, Sc, Sr$  respectively.
5. Bolus size and number of streamlines lowered for the straight channel, but raises for  $H$  increases.

**Appendix`**

$$\alpha_2 = 1 - \sqrt{1 + H^2}, \alpha_1 = 1 + \sqrt{1 + H^2}, \alpha_3 = (h_2 + k)(h_1 + k)^{\alpha_1 - 1} - (h_1 + k)(h_2 + k)^{\alpha_1 - 1},$$

$$\alpha_4 = (h_2 + k)(h_1 + k)^{\alpha_2 - 1} - (h_1 + k)(h_2 + k)^{\alpha_2 - 1}, \alpha_5 = \frac{(h_2 + k)^{\alpha_1} - (h_1 + k)^{\alpha_1}}{\alpha_1},$$

$$\alpha_6 = \frac{(h_2 + k)^{\alpha_2} - (h_1 + k)^{\alpha_2}}{\alpha_2}, \alpha_7 = (h_2 - h_1) \left( k + \frac{h_2 + h_1}{2} \right), \alpha_8 = F(h_1 + k) + \alpha_7,$$

$$\alpha_9 = \alpha_5 (h_1 + k) - \alpha_7 (h_1 + k)^{\alpha_1 - 1}, \alpha_{10} = \alpha_6 (h_1 + k) - \alpha_7 (h_1 + k)^{\alpha_2 - 1},$$

$$c_1 = \frac{1}{\alpha_1} \frac{\alpha_{10} (h_1 - h_2) - \alpha_4 \alpha_8}{\alpha_3 \alpha_{10} - \alpha_4 \alpha_9} = \alpha_{11}, c_2 = \frac{1}{\alpha_2} \frac{\alpha_8 - \alpha_9 \alpha_{11}}{\alpha_{10}} = \alpha_{12}, c_3 = \frac{1}{\alpha_3} \frac{F - \alpha_5 \alpha_{11} - \alpha_6 \alpha_{12}}{\alpha_{17}},$$

$$c_4 = \frac{F}{2} - \left( \frac{c_1 (h_2 + k)^{\alpha_1}}{\alpha_1} + \frac{c_2 (h_2 + k)^{\alpha_2}}{\alpha_2} + c_3 \left( h_2 k + \frac{h_2^2}{2} \right) \right),$$

$$l_1 = c_1 (\alpha_1 - 2) (1 + H^2),$$

$$l_2 = c_2 (\alpha_2 - 2) (1 + H^2)$$

$$C_{11} = \frac{I - \frac{Br}{(1+H^2)^2(-1+Pr DuScSr)} \left\{ \frac{(2H^2 l_1 + l_1^2)}{1+H^2} \left[ (h_2+k)^{\sqrt{1+H^2}} - (h_1+k)^{\sqrt{1+H^2}} \right] + \frac{(2H^2 l_2 + l_2^2)}{1+H^2} \left[ (h_2+k)^{-\sqrt{1+H^2}} - (h_1+k)^{-\sqrt{1+H^2}} \right] + \frac{H^4}{2} \left[ \log(h_2+k)^2 - \log(h_1+k)^2 \right] + 2l_1 l_2 \frac{(h_1-h_2)}{(h_2+k)(h_1+k)} \right\}}{\log(h_2+k) - \log(h_1+k)}$$

$$c_{12} = I - \left\{ c_{11} \log(h_2+k) + \frac{Br}{(1+H^2)^2(-1+Pr DuScSr)} \left[ (l_1^2 + 2H^2 l_1) \frac{(h_2+k)^{\sqrt{1+H^2}}}{1+H^2} + (l_2^2 + H^2 l_2) \frac{(h_2+k)^{-\sqrt{1+H^2}}}{1+H^2} + \frac{2l_1 l_2}{h_2+k} + \frac{H^4 \log(h_2+k)^2}{2} \right] \right\}$$

$$C_{21} = \frac{I - \frac{BrScSr}{(1+H^2)^2(-1+Pr DuScSr)} \left\{ \frac{(2H^2 l_1 + l_1^2)}{1+H^2} \left[ (h_2+k)^{\sqrt{1+H^2}} - (h_1+k)^{\sqrt{1+H^2}} \right] + \frac{(2H^2 l_2 + l_2^2)}{1+H^2} \left[ (h_2+k)^{-\sqrt{1+H^2}} - (h_1+k)^{-\sqrt{1+H^2}} \right] + \frac{H^4}{2} \left[ \log(h_2+k)^2 - \log(h_1+k)^2 \right] + 2l_1 l_2 \frac{(h_1-h_2)}{(h_2+k)(h_1+k)} \right\}}{\log(h_2+k) - \log(h_1+k)}$$

$$c_{22} = I - \left\{ c_{11} \log(h_2+k) + \frac{BrScSr}{(1+H^2)^2(-1+Pr DuScSr)} \left[ (l_1^2 + 2H^2 l_1) \frac{(h_2+k)^{\sqrt{1+H^2}}}{1+H^2} + (l_2^2 + H^2 l_2) \frac{(h_2+k)^{-\sqrt{1+H^2}}}{1+H^2} + \frac{2l_1 l_2}{h_2+k} + \frac{H^4 \log(h_2+k)^2}{2} \right] \right\}$$

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